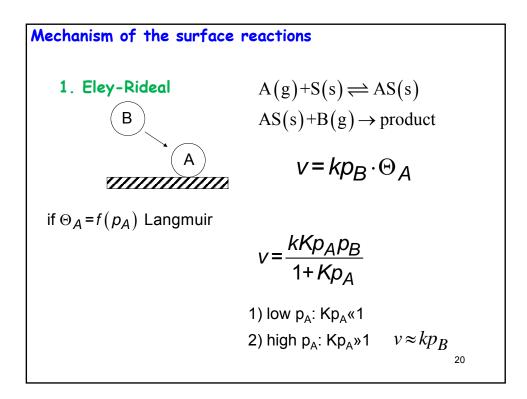
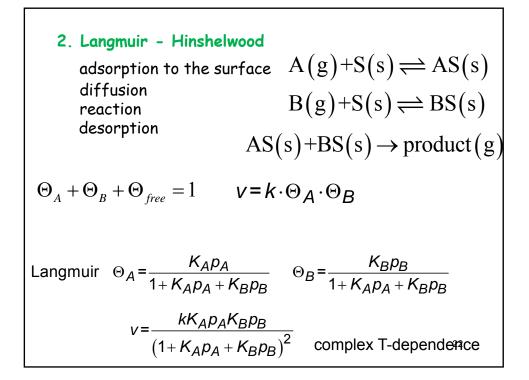
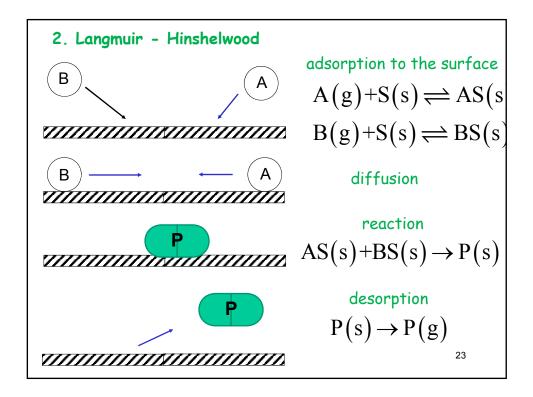


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	1			
process	reagents	catalyst	product	
Ammonia synth.	$N_2+H_2$	Al <sub>2</sub> O <sub>3</sub>	NH <sub>3</sub>	
(Haber-Bosch)		supported		
Ethylono ovido	C <sub>2</sub> H <sub>4</sub> +O <sub>2</sub>	iron oxides	C₂H₄O	
Ethylene oxide synth.	0 <sub>2</sub> n <sub>4</sub> +0 <sub>2</sub>	Al <sub>2</sub> O <sub>3</sub> supported	C <sub>2</sub> Π <sub>4</sub> O	
Synth.		silver		
Desulphurization	H <sub>2</sub> +R <sub>2</sub> S	Al <sub>2</sub> O <sub>3</sub>	RH + H₂S	
of mineral oil	2 2 -	supported	2 -	
		Mo-Co		
Polymerization of	propylene	MgCl <sub>2</sub>	polypropylene	
olephines		supported		
(Ziegler-Natta)		TiCl₃		



reagent	catalyst	product
0 <sub>2</sub> + H <sub>2</sub> (s)		H <sub>2</sub> O + CO
C <sub>2</sub> H <sub>2</sub> + H <sub>2</sub> (s)	Fe or Ni	C <sub>2</sub> H <sub>4</sub>
2 NH <sub>3</sub> + ½ O <sub>2</sub> (s)	Pt	N <sub>2</sub> + 3 H <sub>2</sub> O
C <sub>2</sub> H <sub>4</sub> + ½ O <sub>2</sub> (s)		H <sub>2</sub> COCH <sub>2</sub>





$$\Theta_{A} + \Theta_{B} + \Theta_{szabad} = 1$$

$$V = k \cdot \Theta_{A} \cdot \Theta_{B}$$
Langmuir 
$$\Theta_{A} = \frac{K_{A}p_{A}}{1 + K_{A}p_{A} + K_{B}p_{B}}$$

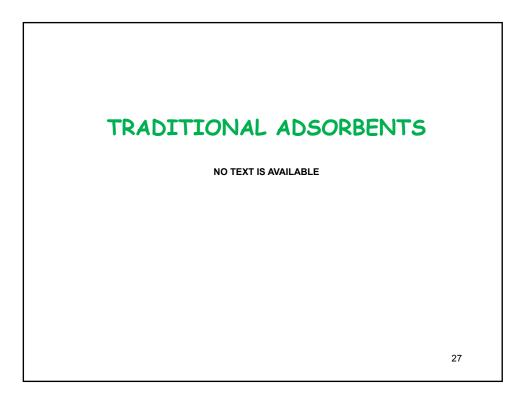
$$\Theta_{B} = \frac{K_{B}p_{B}}{1 + K_{A}p_{A} + K_{B}p_{B}}$$

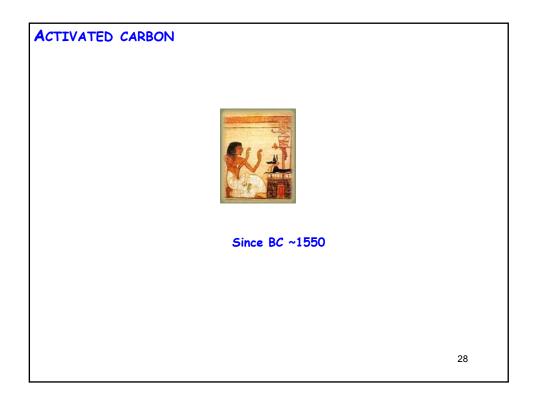
$$V = \frac{kK_{A}p_{A}K_{B}p_{B}}{(1 + K_{A}p_{A} + K_{B}p_{B})^{2}} \quad \text{complex $T$-dependence}$$

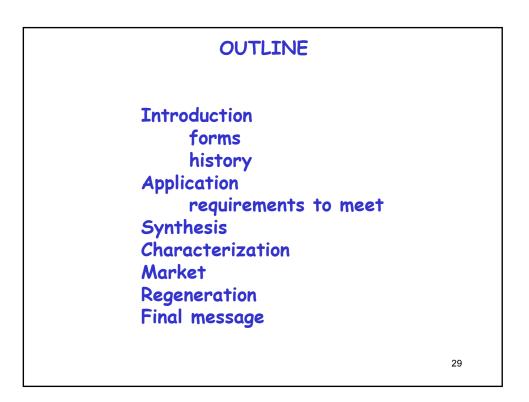
$$24$$

$$v = \frac{kK_A p_A K_B p_B}{(1 + K_A p_A + K_B p_B)^2}$$
  
a) Both A and B adsorb weakly  
$$v = kK_A p_A K_B p_B$$
  
b) B adsorbs weakly  
$$v = \frac{kK_A p_A K_B p_B}{(1 + K_A p_A)^2}$$
  
c) A adsorbs very strongly  
$$v = \frac{kK_B p_B}{1 + K_A p_A}$$

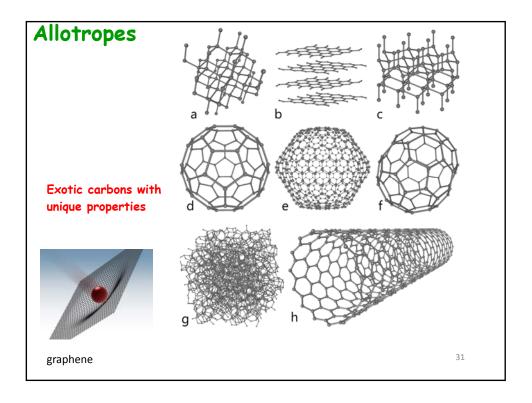
Lonomu	in Linchel			
Langmu	ir - Hinshel	wooa examp	Dies	
			· · · · · · · · · · · · · · · · · · ·	
	reagents	catalyst	product	
	2 CO + O <sub>2</sub>	platinum	2CO <sub>2</sub>	
	CO + 2H <sub>2</sub>	ZnO	CH₃OH	
	$C_2H_4 + H_2$	copper	C <sub>2</sub> H <sub>6</sub>	
	$N_{2}O + H_{2}$	platinum	$N_2 + H_2O$	
	$C_2H_4 + \frac{1}{2}O_2$	palladium	CH <sub>3</sub> CHO	
	CO + OH	platinum	CO <sub>2</sub> + H <sup>+</sup> + e <sup>-</sup>	
				26







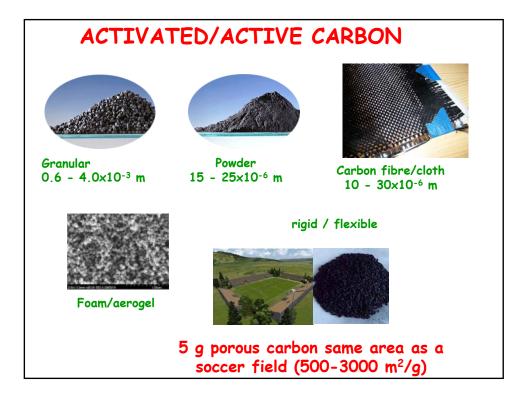


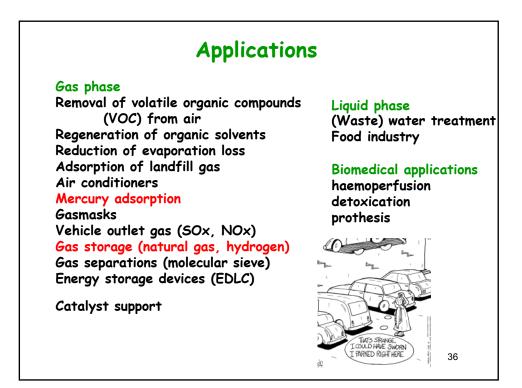


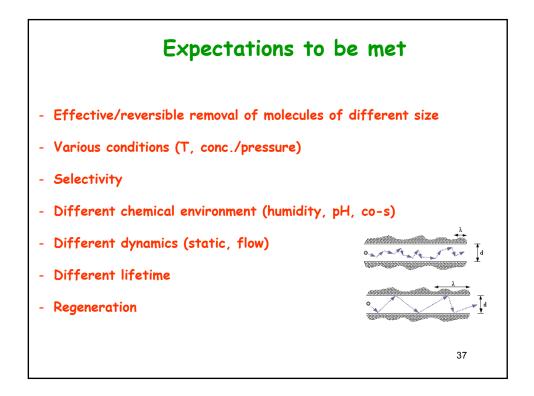
A LITTL	E HISTORY	/
	BC 3750	Egypt, Mesopotamia
Res it	1789	element (Lavoisier)
	1961	IUPAC ( <sup>12</sup> C atomic mass unit)
	1960	W. Libby
	1991	S. Iijima CNT (1952 Radushkevich) Nobel nomination
	1994	G. Oláh
	1996	R. F. Curl Jr. Sir H. W. Kroto R. E. Smalley
	2010	A. Geim, K. Novoselov
		http://www.nobelprize.org/

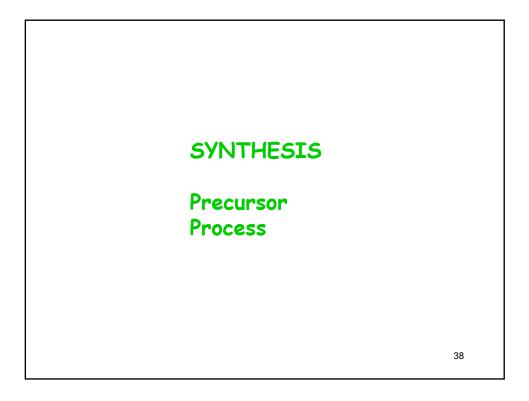


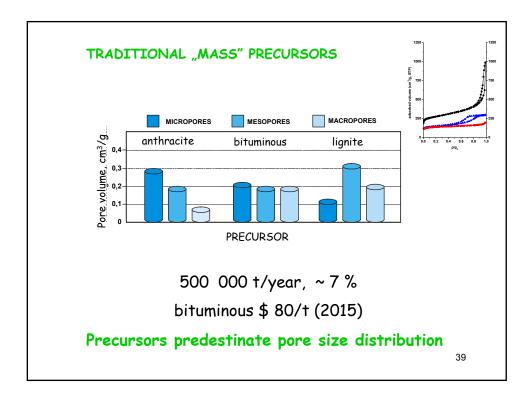
"Activated carbon, characterized by its exceptional adsorption properties, has been identified as an effective solution for air and water pollution control, which is driving its demand in both mature and emerging markets across the globe. Besides drinking water treatment and air purification, activated carbon is also actively used in controlling mercury emissions, caused by burning of coal in power plants. With growing use in diverse end user industries, such as mining, food & pharmaceuticals and chemical beverage. & petrochemical, the global market for activated carbon is expected to post strong growth over the next five years." (Global Activated Carbon Market Forecast and **Opportunities**, 2019) 34

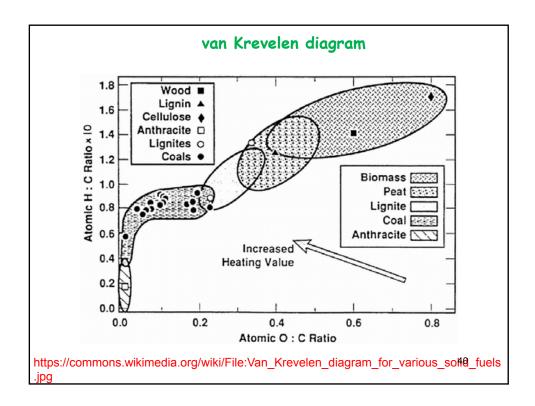


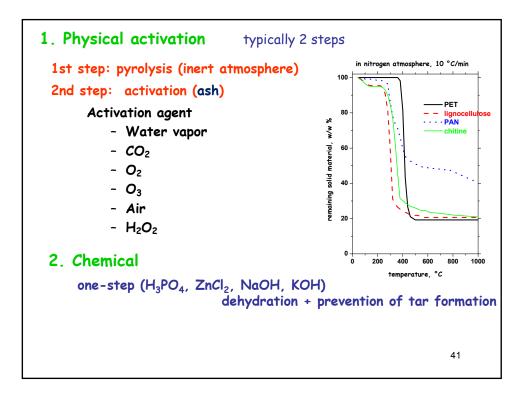


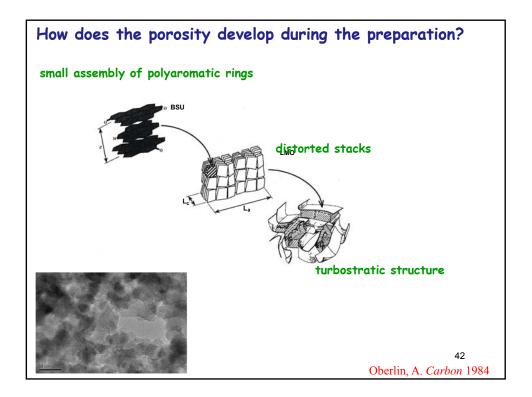


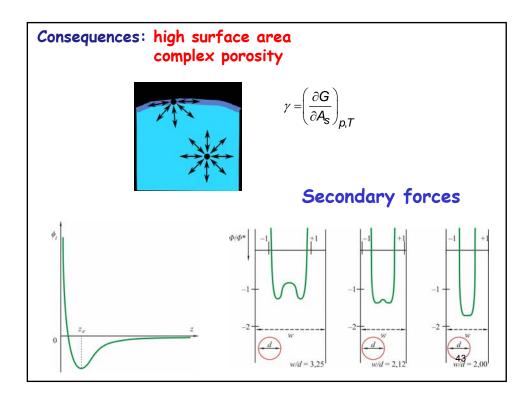


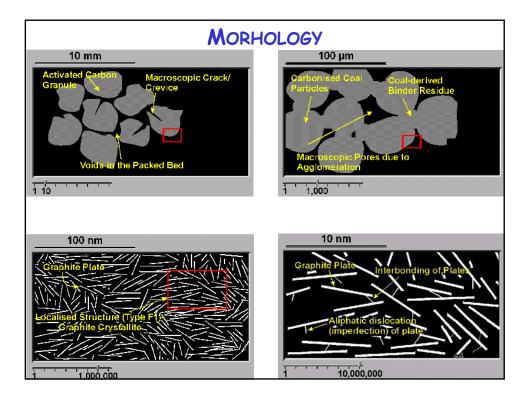


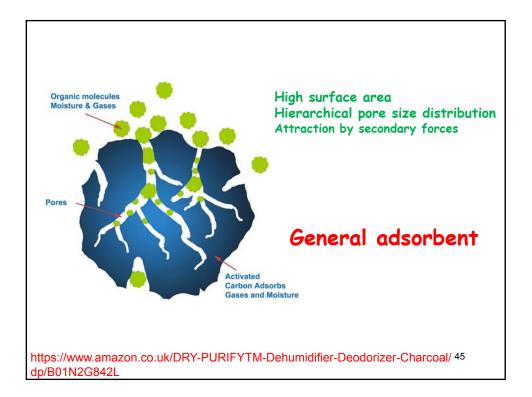


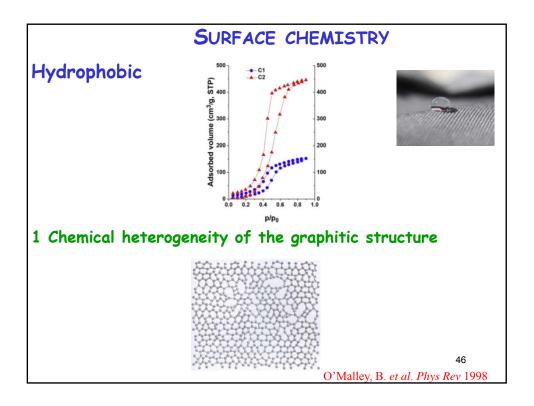


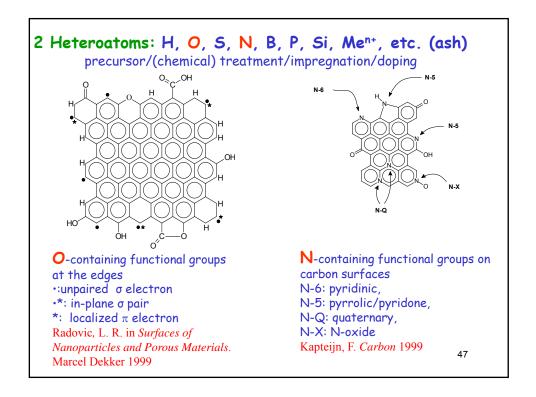


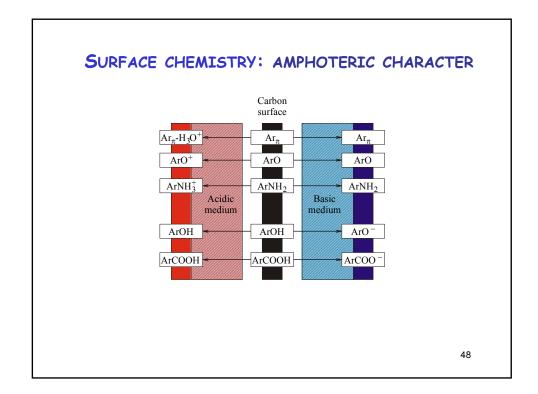


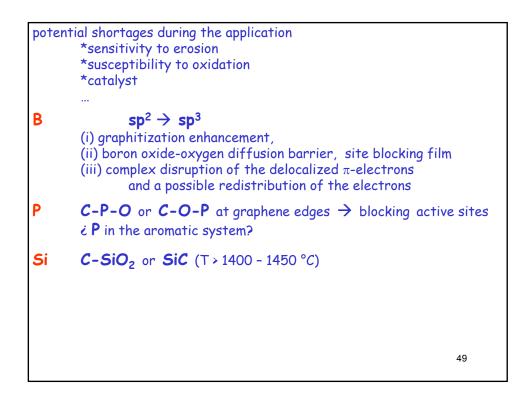










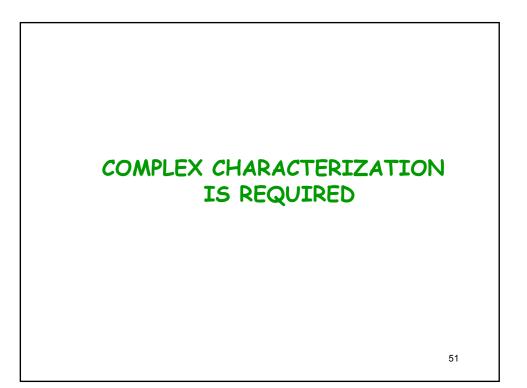


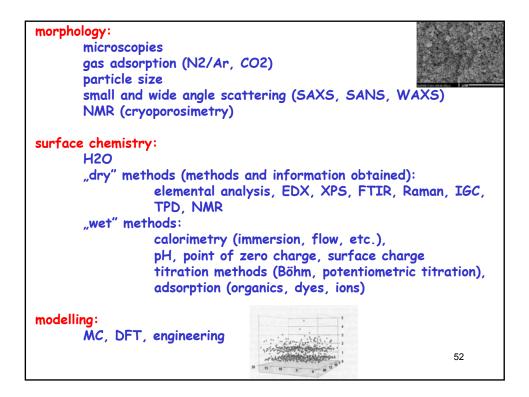


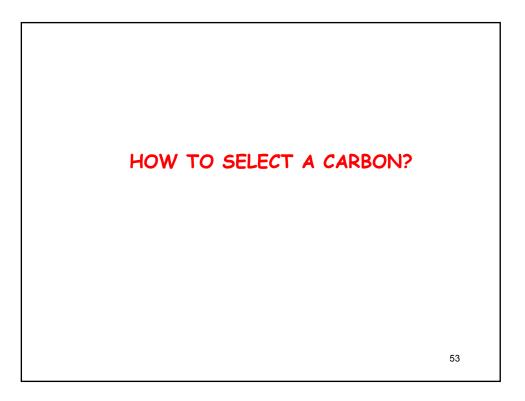
# Impregnation

Sensitize for a limited number of target chemicals (vs catalyst support)

iodine silver Al, Mn, Zn, Fe, Li, Ca transient metals: Cu, Mo, etc.

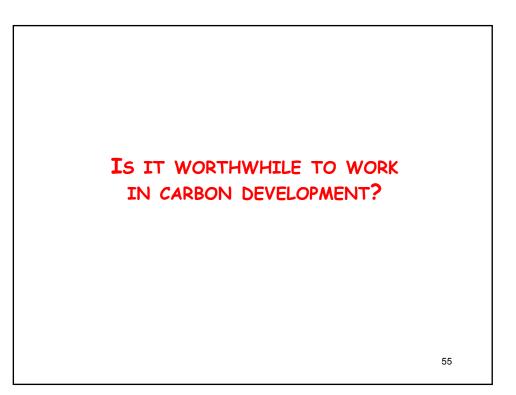


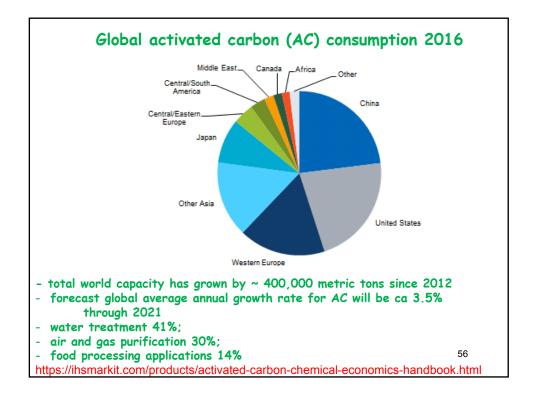


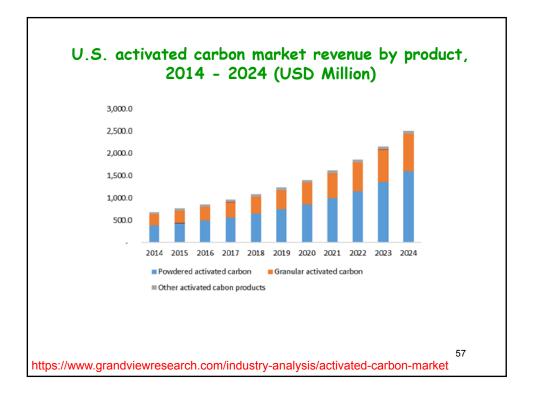


## Application oriented standardized test methods AS CLOSE AS POSSIBLE TO APPLICATION CONDITIONS

BET surface area, PSD Iodine number Molasses Phenol uptake Methylene blue Dechlorination Apparent density Hardness/abrasion number Ash content Carbon tetrachloride activity Particle size distribution







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### Regeneration of activated carbon (vs. hazardous waste)

#### Thermal regeneration

about 800 °C, controlled atmosphere widely used disadvantages: high cost energy intensive high carbon losses

### Further regeneration techniques

Chemical and solvent regeneration Microbial regeneration Electrochemical regeneration Ultrasonic regeneration Wet air oxidation

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area : activity
s donor exchange
60

